



State of the Art and Challenges in Polymer Electrolyte Fuel Cell Membranes

NIST NCMC-14 Meeting

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James Goldbach

Arkema, Inc.

King of Prussia, PA 19406

Outline

- Fuel Cell Types and Related Separators
- PEM Fuel Cell Types
 - Hydrogen PEMFC
 - Direct Methanol PEMFC
 - Other: Alkaline, Alternative Fuels
- Membrane Requirements
- PFSA Membranes
- Hydrocarbon Membranes
- Challenges and Future Directions

Fuel Cell Types

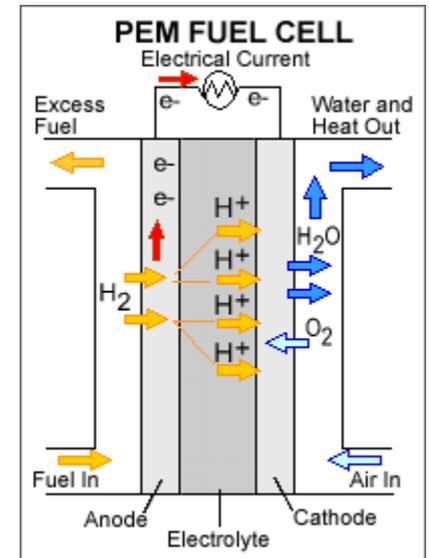
Fuel Cell Type	Common Electrolyte	Operating Temperature	System Output	Electrical Efficiency	Applications	Advantages	Disadvantages
Polymer Electrolyte Membrane (PEM)*	Solid organic polymer poly-perfluorosulfonic acid	50 - 100°C 122 - 212°F	<1kW – 250kW	53-58% (transportation) 25-35% (stationary)	<ul style="list-style-type: none"> Backup power Portable power Small distributed generation Transportation 	<ul style="list-style-type: none"> Solid electrolyte reduces corrosion & electrolyte management problems Low temperature Quick start-up 	<ul style="list-style-type: none"> Requires expensive catalysts High sensitivity to fuel impurities Waste heat temperature not suitable for combined heat and power (CHP)
Alkaline (AFC)	Aqueous solution of potassium hydroxide soaked in a matrix	90 - 100°C 194 - 212°F	10kW – 100kW	60%	<ul style="list-style-type: none"> Military Space 	<ul style="list-style-type: none"> Cathode reaction faster in alkaline electrolyte, leads to higher performance 	<ul style="list-style-type: none"> Expensive removal of CO₂ from fuel and air streams required (CO₂ degrades the electrolyte)
Phosphoric Acid (PAFC)	Liquid phosphoric acid soaked in a matrix	150 - 200°C 302 - 392°F	50kW – 1MW (250kW module typical)	>40%	<ul style="list-style-type: none"> Distributed generation 	<ul style="list-style-type: none"> Higher overall efficiency with CHP Increased tolerance to impurities in hydrogen 	<ul style="list-style-type: none"> Requires expensive platinum catalysts Low current and power Large size/weight
Molten Carbonate (MCFC)	Liquid solution of lithium, sodium, and/or potassium carbonates, soaked in a matrix	600 - 700°C 1112 - 1292°F	<1kW – 1MW (250kW module typical)	45-47%	<ul style="list-style-type: none"> Electric utility Large distributed generation 	<ul style="list-style-type: none"> High efficiency Fuel flexibility Can use a variety of catalysts Suitable for CHP 	<ul style="list-style-type: none"> High temperature speeds corrosion and breakdown of cell components Complex electrolyte management Slow start-up
Solid Oxide (SOFC)	Yttria stabilized zirconia	600 - 1000°C 1202 - 1832°F	<1kW – 3MW	35-43%	<ul style="list-style-type: none"> Auxiliary power Electric utility Large distributed generation 	<ul style="list-style-type: none"> High efficiency Fuel flexibility Can use a variety of catalysts Solid electrolyte reduces electrolyte management problems Suitable for CHP Hybrid/GT cycle 	<ul style="list-style-type: none"> High temperature enhances corrosion and breakdown of cell components Slow start-up Brittleness of ceramic electrolyte with thermal cycling

*Direct Methanol Fuel Cells (DMFC) are a subset of PEM typically used for small portable power applications with a size range of about a subwatt to 100W and operating at 60 - 90°C.

PEM Fuel Cells

- Polymer Electrolyte Membrane Fuel Cells

- H₂ or methanol fuel
 - Stored, or from reformed hydrocarbons
- Relatively low temperature operation
 - 60-90 °C is typical
 - 80 °C for H₂ PEM
- Solid polymer separator (membrane)
 - Proton conductive
 - Mechanically strong
 - Hydrolytically and oxidatively stable
 - Low in-plane swelling
 - Low fuel and oxidant cross-over
 - Electrically insulating
 - Inexpensive (~10m² membrane / vehicle)



PEM Requirements – “A Tough Challenge”

Property	Metric	Typical Value	Material
Proton conductive	4-point <i>ex-situ</i> (hydrated 60-80C) 4-point <i>ex-situ</i> (25% to 90% RH)	160-200mS/cm 5-100mS/cm	PFSA
Mechanically strong	Tensile strength (23°C, 50% RH) Modulus (23°C, 50% RH)	~25 MPa* ~285 MPa*	Nafion®
(Electro)Chemically stable	Time @ OCV (<i>in-situ</i>) ^a	100-200h † 300-400h †	PFSA Hydrocarbon
Low in-plane swelling	(%) \bar{x} -y dimensional swelling	< 5% 15-20%	Reinforced Non-reinforced
Low fuel and gas cross-over	Electrochemical (mA/cm ²)	1.5 mA/cm ² 0.5 mA/cm ²	Nafion® Arkema M41
Inexpensive	\$ <u>retail</u> \$ @ <u>commercial volume</u>	\$465 / m ² ** \$20 / m ² ***	Nafion®

*DuPont technical data sheet for Nafion® NR-211 membrane.

**Retail price for NR-211 from Ion Power, Inc on 10/29/2008 (www.ion-power.com)

***US DOE target for automotive applications.

† www.hydrogen.energy.gov/pdfs/progress07/v_m_5_foure.pdf

^a Zhang, J., et.al., J. Power Sources, 2006, (163), 532-537.

Membrane Types

- Membrane Chemistry

- PFSA

- Perfluorinated copolymers

- Hydrocarbon

- Aromatic backbone copolymers
 - Aliphatic backbone copolymers
 - Polymer blends
 - Controlled-architecture (block and graft copolymers)

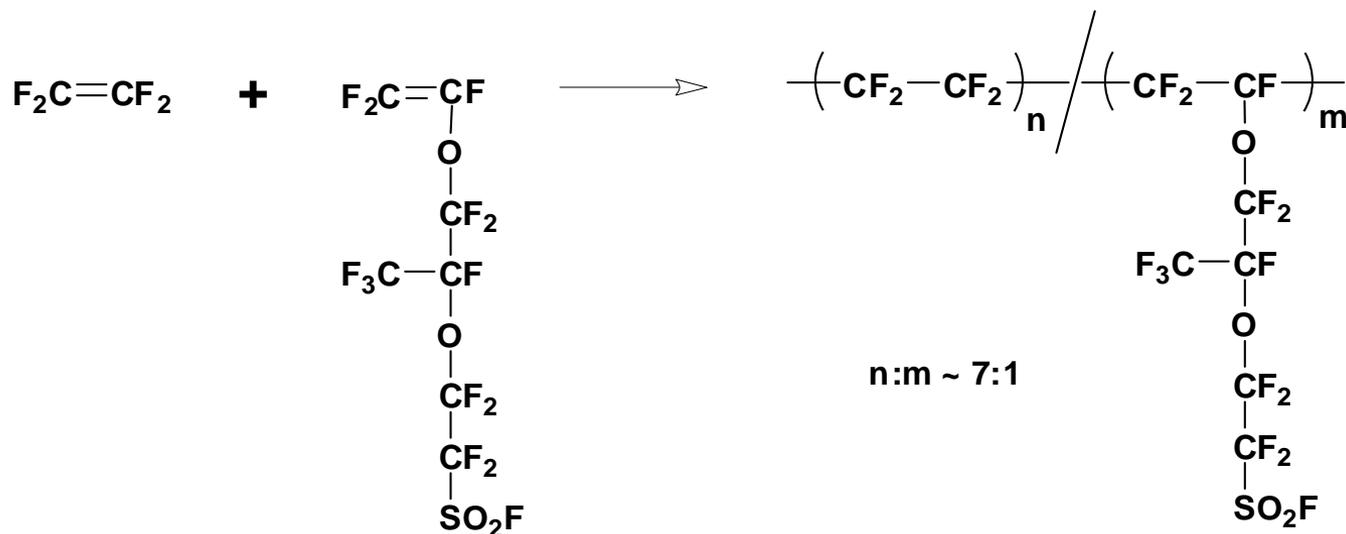
- Application

- H₂ PEM – Stationary
 - H₂ PEM – Automotive
 - H₂ PEM – Portable (backup power)
 - DMFC
-

PFSA Membranes

- Perfluorinated Sulfonic Acid

- Nafion[®]
- A single copolymer
- Developed (1963) for chlor-alkali applications
 - Tetrafluoroethylene + perfluorinated vinyl ether



- EW ~ 1000-1100 g/mol H⁺
- IEC ~ 1.0 – 0.91 molH⁺/g

PFSA Membranes

- Non-Nafion[®] PFSA Materials
 - Similar production process as Nafion[®]
 - Varied side-chain type

	Nafion [®] (DuPont)	Aciplex [®] (Asahi Chemical)	Hyflon [®] Ion (Solvay- Solexis)	Flemion [®] (Asahi Glass)	3M
Side Group	$ \begin{array}{c} \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{F}_3\text{C}-\text{CF} \\ \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{SO}_3\text{H} \end{array} $	$ \begin{array}{c} \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{F}_3\text{C}-\text{CF} \\ \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{SO}_3\text{H} \end{array} $	$ \begin{array}{c} \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{SO}_3\text{H} \end{array} $	$ \begin{array}{c} \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{SO}_3\text{H} \end{array} $	$ \begin{array}{c} \\ \text{O} \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{CF}_2 \\ \\ \text{SO}_3\text{H} \end{array} $
Typical EW	1000-1100	1000-1100	750-900	800-900	800-900

EW = grams of material / mol SO₃H

Grot, W., in "Perfluorinated Ionomers", 2007, ISBN 978-0-8155-1541-8.

R.L. Ames et al. / *Journal of Membrane Science* 249 (2005) 65–73

PFSA Membranes – In-Situ Performance

- Nafion[®] (DuPont)

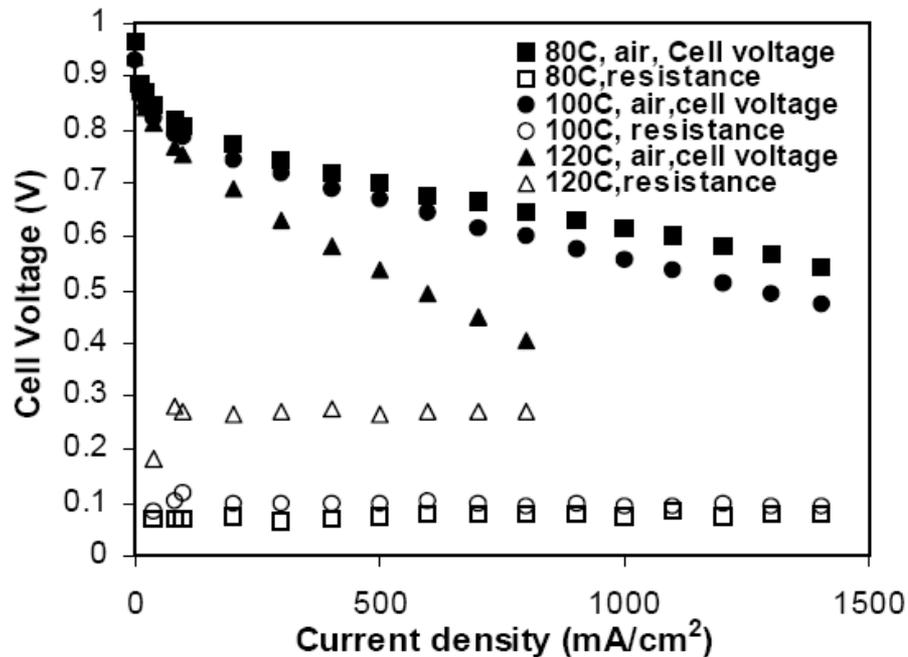


Fig.1 Cell performance at three different conditions at atmospheric pressure on air
Cell temperature was 80°C (75%R.H. cathode), 100°C (70%R.H. cathode) and 120°C (35%R.H.cathode)

PFSA Membranes – State of the Art - Durability

- OCV Hold Accelerated Durability Testing*
 - DOE Protocol*: 90 °C, O₂, OCV, 30% RH
 - Failure Criterion: 20% loss in OCV
 - Chemical degradation leads to membrane thinning
 - Typical PFSA membranes fail in 100-200h

- RH Cycling*
 - DOE Protocol*: 25-50cm² cell, 80°C, cycle air 2min./2min. @ 0/100% RH
 - Failure Criterion: air crossover > 10sccm or 20,000 cycles
 - RH cycling leads to mechanical membrane failure
 - Only 1 PFSA membrane meets 20,000 cycle target (PFSA 111-IP)

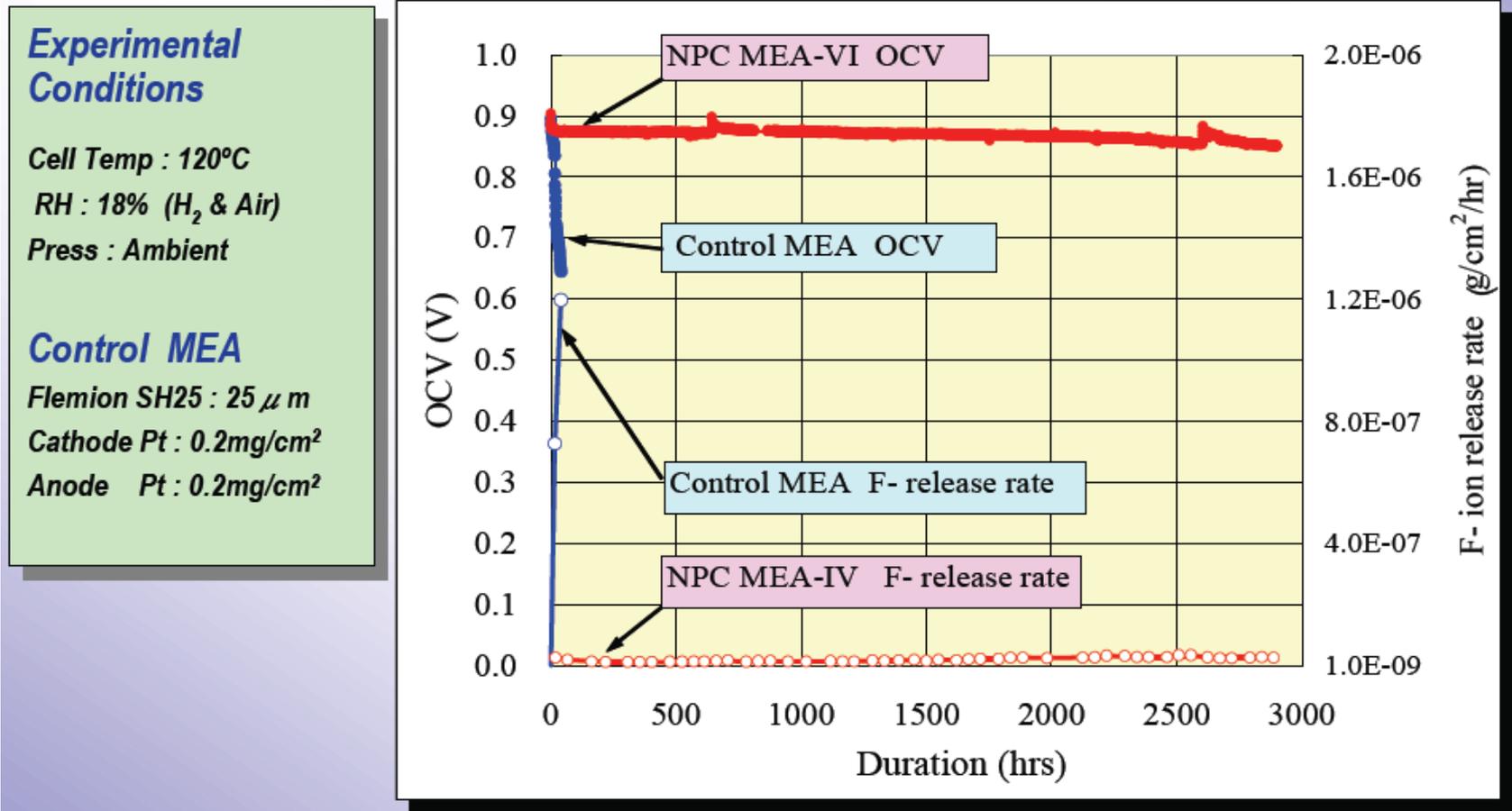
Tang, H., et.al., "A Degradation Study of Nafion Proton Exchange Membrane of PEM Fuel Cells", *J. Power Sources*, **2007**, (170), 85–92.

Schiraldi, D.A., "Perfluorinated Polymer Electrolyte Membrane Durability", *J. Macromol. Sci., Part C: Polym. Rev.*, **2006**, (46), 315–327.

*US DOE testing protocols, Funding Opportunity Announcement DE-PS36-08GO98009 (5/27/2008).

PFSA Membranes – State of the Art – Overall

- Asahi Glass – New ‘NPC’ PFSA Membrane



Endoh, E., "Progress of Highly Durable MEA for PEMFC Under High Temperature and Low Humidity Conditions", 2007 Fuel Cell Seminar Presentation.

PFSA Membranes – “Wish List”

- Low EW Ionomer → Conductivity
- Mechanically Reinforced → Low Swelling
- Stabilized end groups → Chem. Stability
- Redox-active additive → Chem. Stability (*in-situ*)
- High conductivity at low RH → Auto. applications
- Low gas cross-over → High fuel utilization
- Inexpensive (<\$20/m²) → Commercially viable

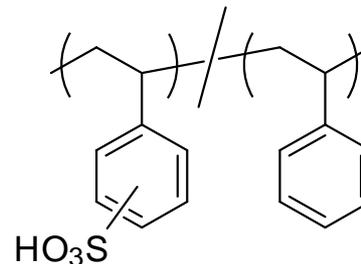
● Low RH conductivity and low cost are difficult for PFSAs

Hydrocarbon Membranes

- Aliphatic Backbones

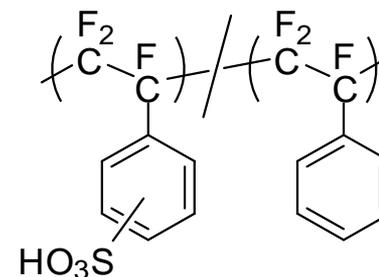
- sPS (GE, 1960s)

- Direct sulfonation of polystyrene
- Very inexpensive, simple to produce
- Oxidatively unstable
- Limited IEC range



- BAM3G (Ballard)

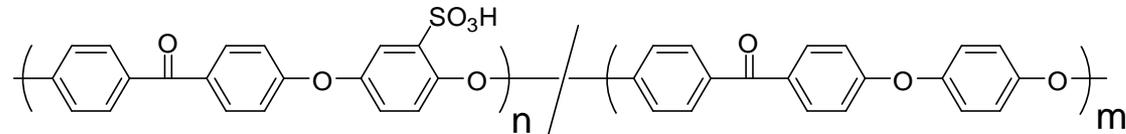
- Copolymerization of α,α,β -trifluorostyrenes
- Better oxidative stability
- Limited IEC range
- Specialized monomer



Hydrocarbon Membranes

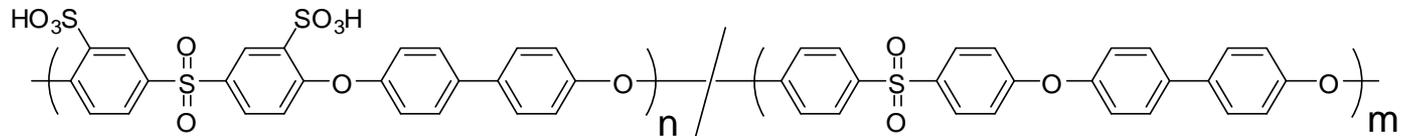
- Aromatic Backbones

- sPEEK



- Direct sulfonation of engineering thermoplastic

- BPSH



- Copolymerization of pre-sulfonated monomers

- Sulfonated polyarylsulfide (sulfone)



- Copolymerization / sulfonation of intermediates

Hydrocarbon Membranes

- Random Copolymers

- Advantages

- Potentially very low cost
 - Increased chemical durability

- Disadvantages

- Direct sulfonation ~ limited *in-situ* stability
 - Pre-sulfonation / copolymerization necessary
 - Limited sulfonate content
 - Swelling / conductivity tradeoff
 - Rapid drop in proton conductivity at reduced RH

- Block Copolymers

- Control size of hydrophilic domains

- Increase local concentration of acidic functionality

Hydrocarbon Membranes

- BPSH Random Copolymers

Y.S. Kim et al. / Journal of Membrane Science 243 (2004) 317–326

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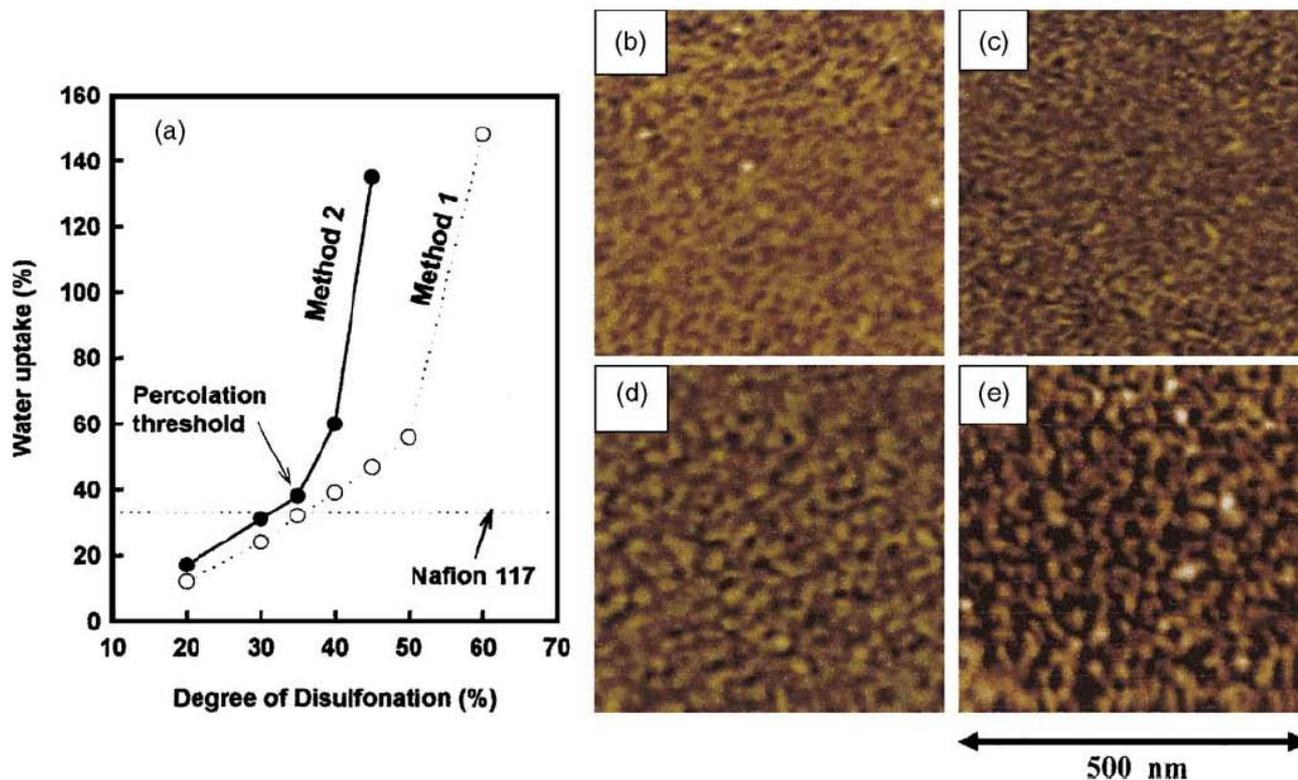


Fig. 4. (a) Percent water uptake and (b)–(e) morphology as a function of degree of disulfonation at 25 °C of BPSH treated by *Method 2* acidification; (b) BPSH-30, (c) BPSH-35, (d) BPSH-40 and (e) BPSH-45. The micrograph (d) was reproduced from [15].

Hydrocarbon Membranes

- Controlled Morphology

- Polymer architecture determines phase-separated morphology

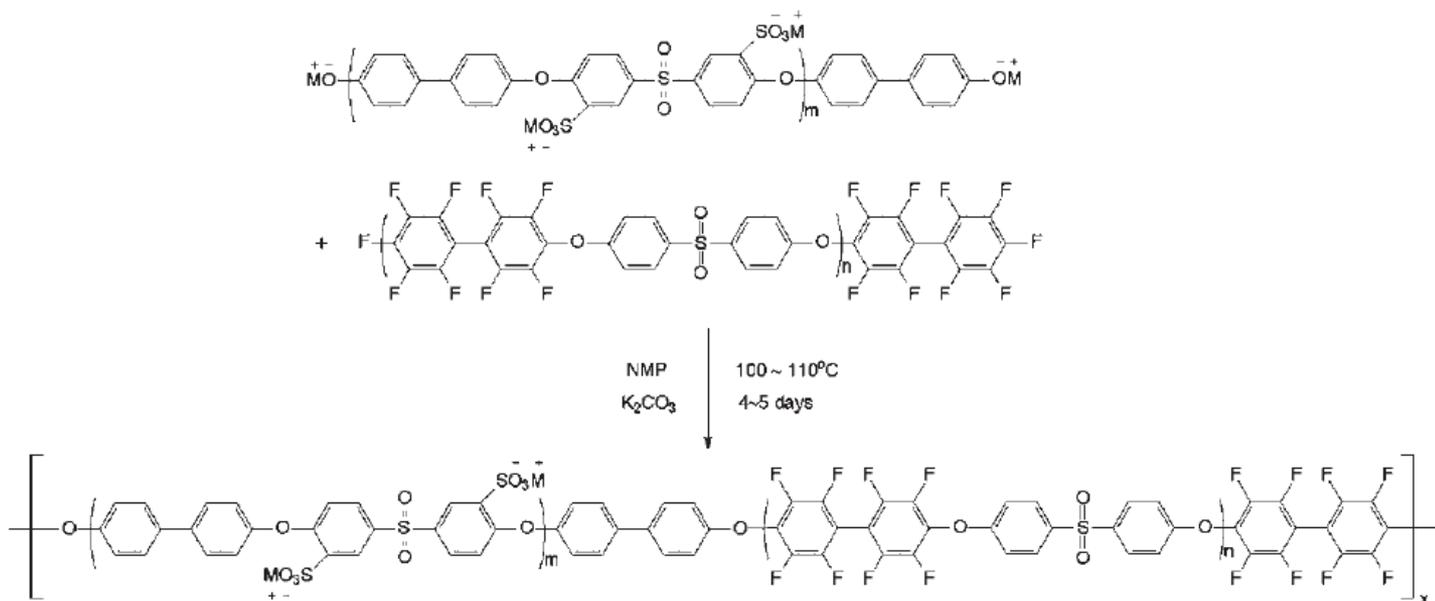


Figure 7.
Synthesis of BisSF-BPSH multiblock copolymers.

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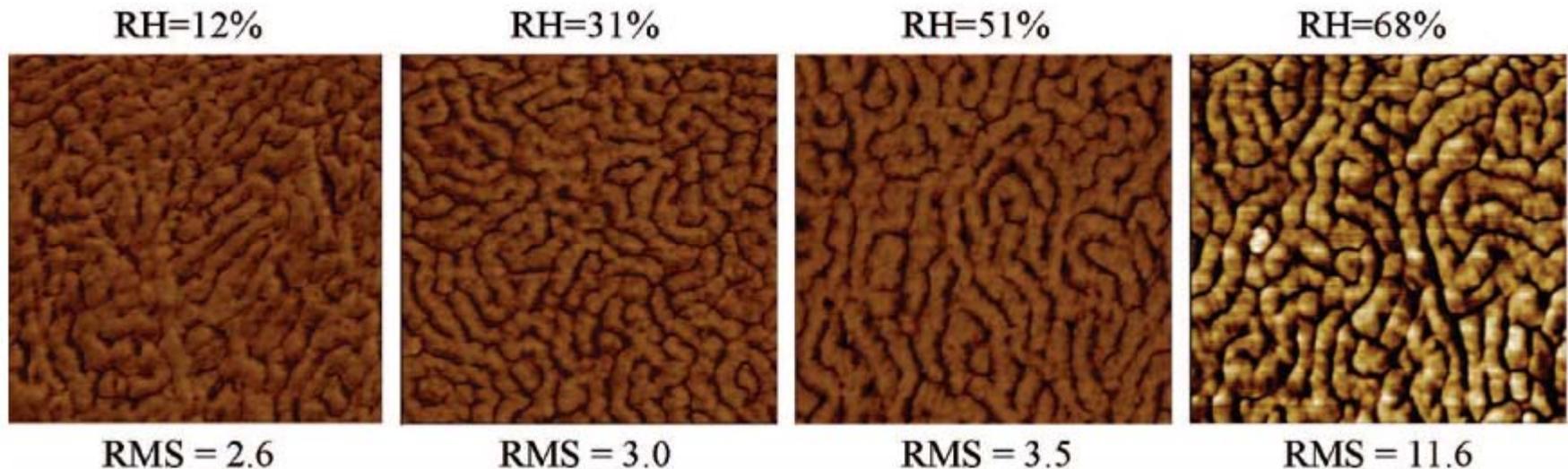
www.ms-journal.de

McGrath, J.E., et al., *Macromol. Symp.*, **2006**, (245-246), 439-449.

Hydrocarbon Membranes

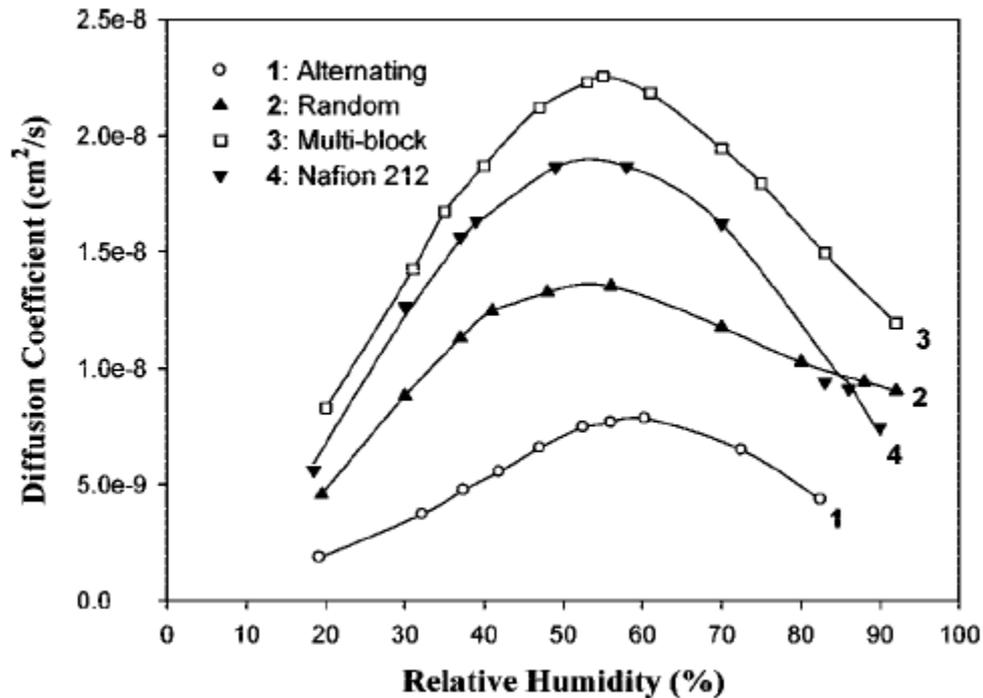
- Controlled Morphology

- Polymer architecture determines phase-separated morphology
- BPSH block copolymers



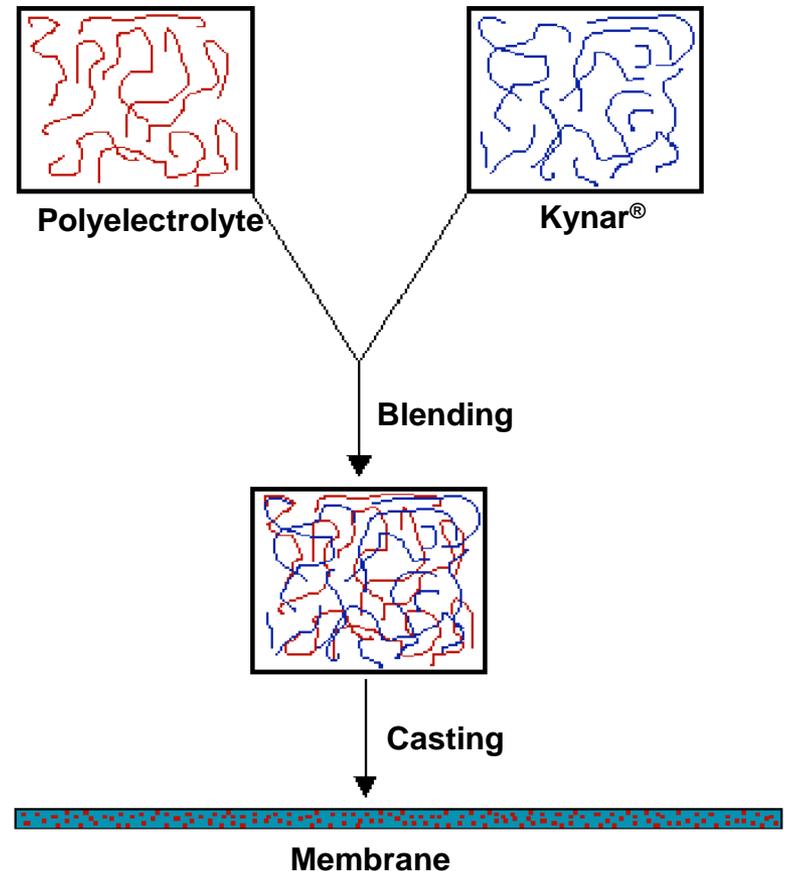
Hydrocarbon Membranes

- Water diffusion coefficient comparison for BPSH materials
- Critical for proton transport

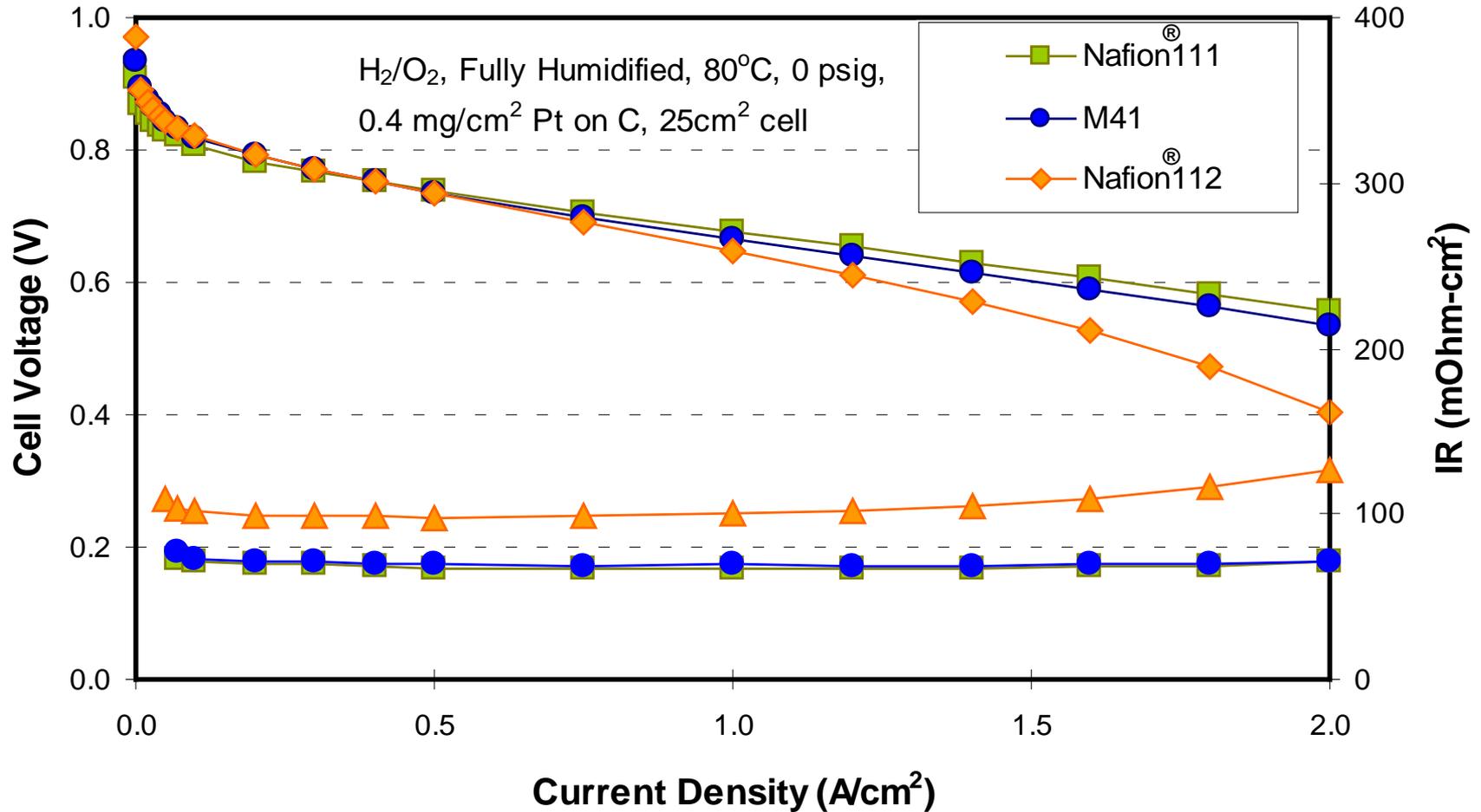


Hydrocarbon Membranes – Arkema's Approach

- Polymer blend system
- Decouple proton conductivity from mechanical requirements
 - Kynar[®] PVDF
 - Commercial product
 - Mechanical support
 - Chemical resistance
 - Electrochemical stability
 - Polyelectrolyte
 - H⁺ conduction
- Process Flexibility
- A lower-cost approach
 - Kynar[®] PVDF - commercial product
 - Polyelectrolyte – minor component

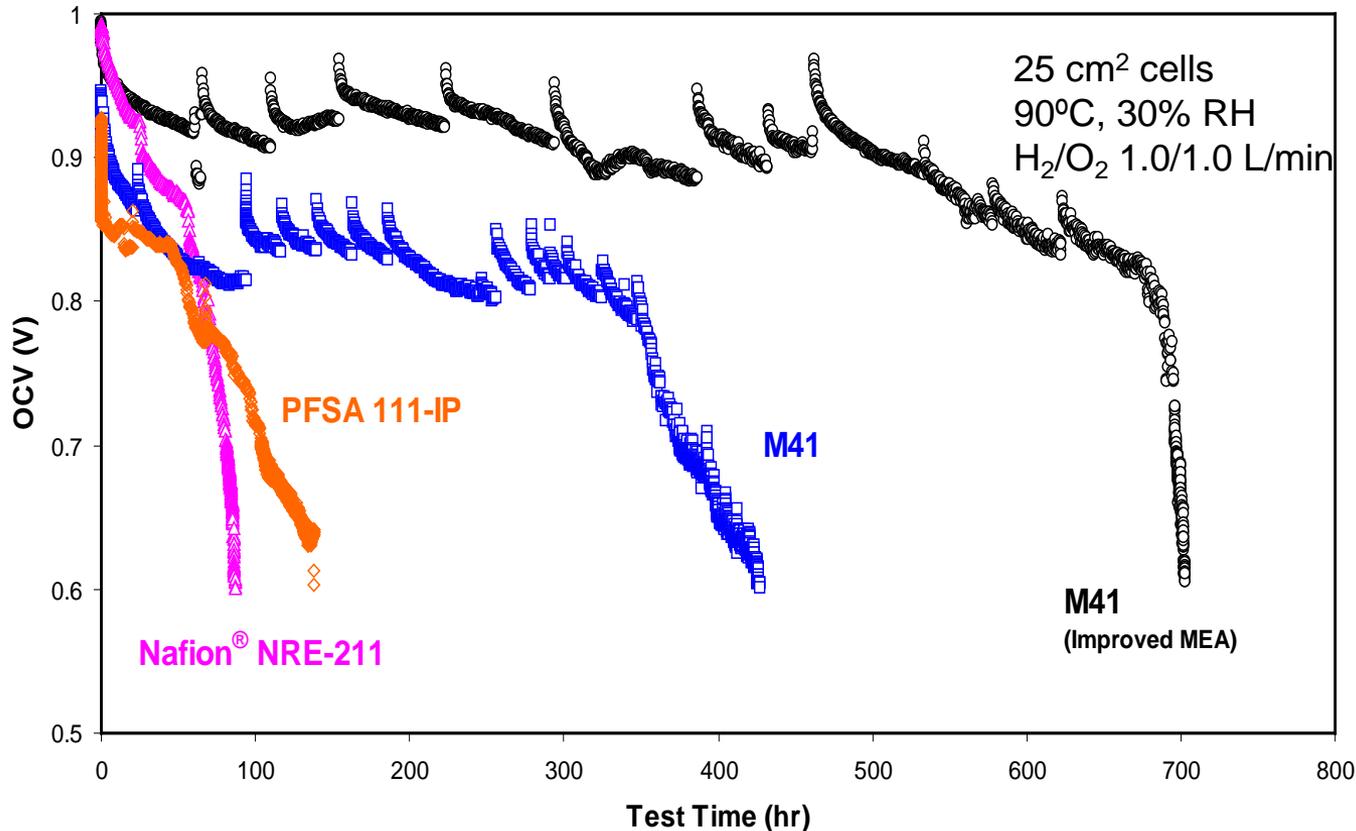


Arkema M41: BOL Performance



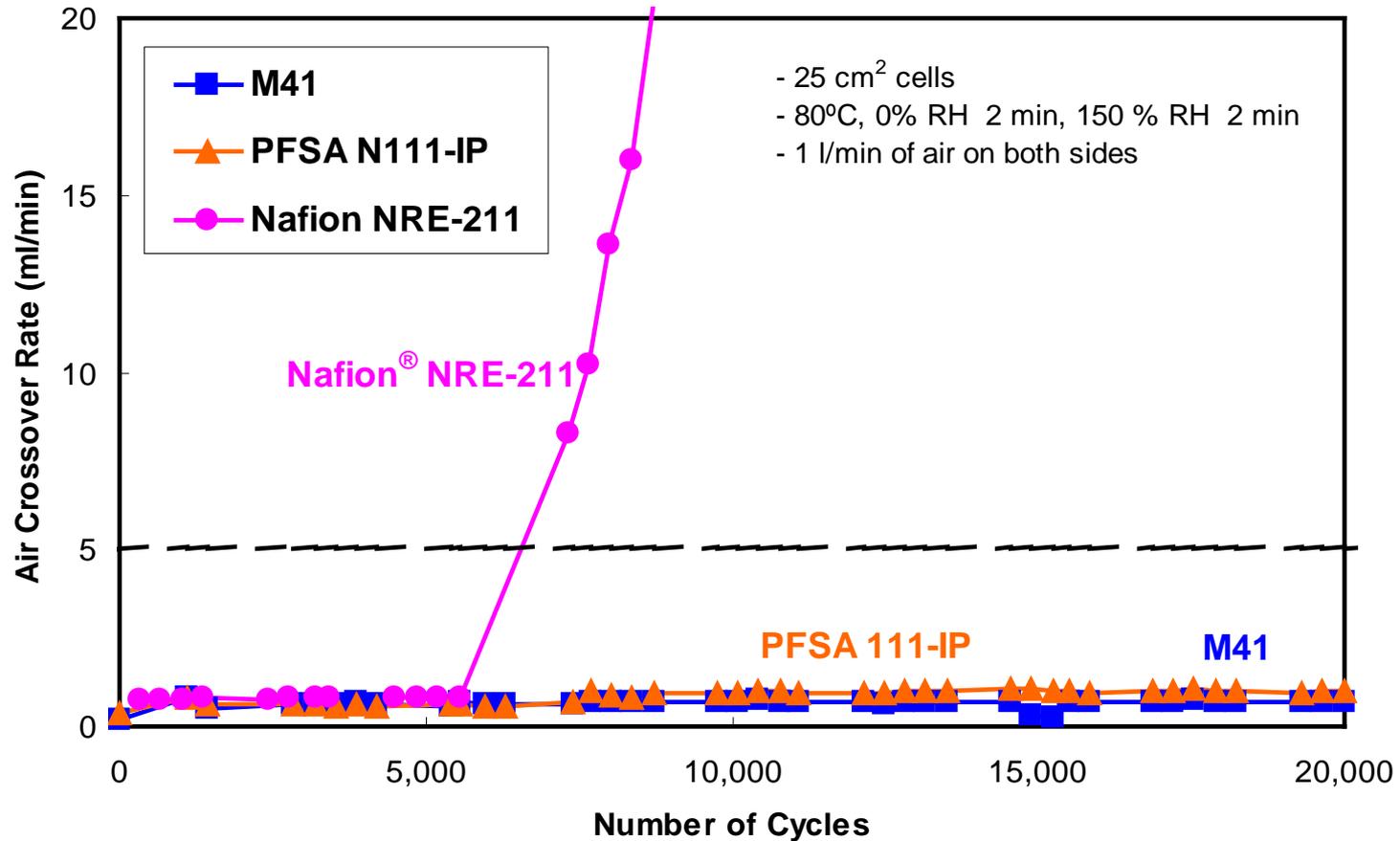
- Comparable in-cell performance to Nafion[®] 111 demonstrated

Arkema M41 – OCV Durability



- Short resistance decreases for PFSA and M41 membranes
- No fluoride and low sulfate emission from M41
- H₂ cross-over remains very low at failure for M41
- Fluoride emission and H₂ cross-over from PFSAs

Arkema M41: RH Cycling



- Nafion[®] NRE-211 failed at approximately 6,000 cycles
- M41 and PFSA 111-IP MEAs met target of 20,000 cycles
- M43 (improved M41 MEA) has exceeded 50,000 cycles

State of the Art – Availability

- PFSA Membranes

- Nafion[®] (DuPont) - Widely available
 - Distributed in film and dispersion form
 - www.ion-power.com
 - Hyflon[®] Ion
 - Available from manufacturer - Solvay-Solexis
 - Flemion[®]
 - Aciplex[®]
 - 3M Ionomer
- Not as widely distributed

- Hydrocarbon Membranes

- PolyFuel Inc. – DMFC membranes to OEMs only
- Arkema – to customers/collaborators under NDA only
- BPSH – University project(s) – not commercial scale

State of the Art – All Membranes

- PFSA Membranes

- Asahi Glass – NPC PFSA
- Nafion[®] XL – reinforced Nafion[®] PFSA

- Hydrocarbon Membranes

- BPSH block copolymer membranes (VA Tech, J. McGrath)
- Arkema – M41 PVDF blend membranes
- FumaTECH – FumaPEM P,E,K series membranes
- PolyFuel Inc. – DMFC membranes

PEM Requirements – “The Automotive Challenge”

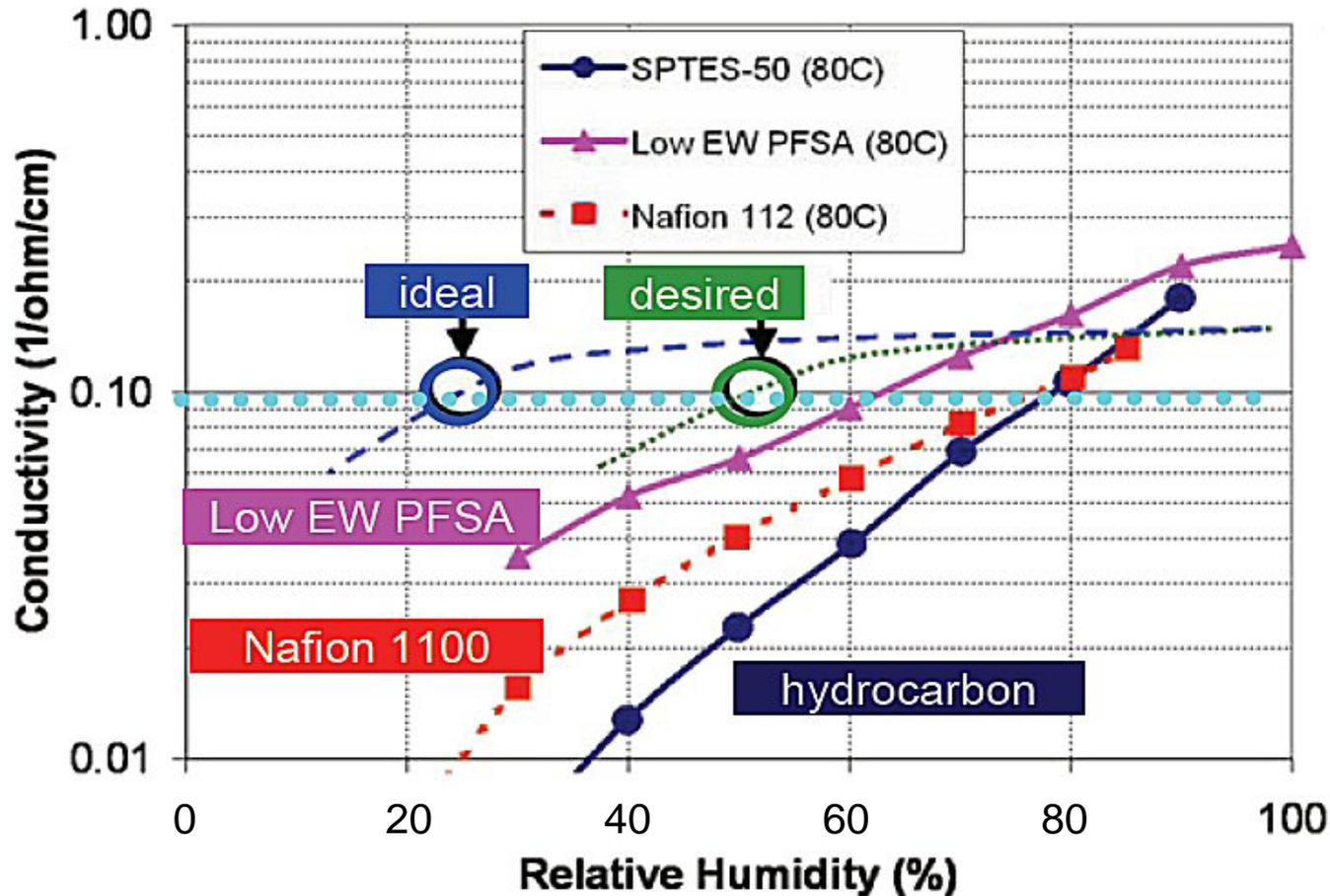
Characteristics	Units	Calendar year		
		2000 status ^a	2005	2010
Membrane conductivity, operating temperature	$\Omega\text{-cm}^{-1}$	0.1	0.1	0.1
Room temperature	$\Omega\text{-cm}^{-1}$			
-20° C	$\Omega\text{-cm}^{-1}$			
Oxygen cross-over ^b	mA/cm^2	5	5	2
Hydrogen cross-over ^b	mA/cm^2	5	5	2
Cost	\$/kW		50	5
Operating Temperature	°C	80	120	120
Durability	Hours	1000 ^d	>4000 ^e	>5000 ^f
Survivability ^c	°C	-20	-30	-40
Thermal cyclability in presence of condensed water		yes	yes	yes

Notes:

- a) Status is present day 80°C unless otherwise noted; targets are for new membranes/CCMs
- b) Tested in CCM
- c) Indicates temperature from which bootstrapping stack must be achieved
- d) Continuous operation
- e) Includes thermal cycling
- f) Includes thermal and realistic driving cycles

PEM Requirements – “The Automotive Challenge”

- Proton Conductivity



US DOE HFCIT – High Temperature Membrane Working Group presentation – T. Greszler, “Membrane Performance and Durability Overview for Automotive Fuel Cell Applications”, September 14, 2006.



Summary

- PEM fuel cell membranes must meet many challenges
- Nafion[®] is widely-distributed
- Alternatives in varying degrees of commercialization
- Many chemistries possible with hydrocarbon materials
- Application defines membrane properties
 - Automotive – stringent performance and durability requirements
 - Stationary / Backup – durability is critical
 - Portable – high fuel utilization is critical (DMFC)
- Rapid property screening and optimization needed
- **LOW COST** will be the key!